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Hot Corrosion of Aluminized 1020 Steel with NaCI Deposit

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Abstract. The oxidation of hot-dip aluminized AISI 1020 steel coated with NaCl in static air at 700 °C for a duration of time 49 h was studied by employing thermogravimetry, Scanning Electron Microscopy (SEM), Electron Dispersive Spectroscopy (EDS) and X-ray Diffraction (XRD) analysis. It was found that NaCl deposits markedly accelerated the oxidation of the AISI 1020 steel. The aluminide coating on the bare steel gives the best oxidation protection by forming continuous alumina scale (Al₂O₃). The degradation of aluminide layer and alumina scale on the steel are associated by chloridation/oxidation cyclic reactions. In addition, the released chlorine will be as catalytic actions and leads to the formation of loose Al₂O₃ during corrosion.

Introduction

Comterical AISI 1020 steel can be considered as a candidate material for the use of pipelines system in the Geothermal Power Plant in Ulubelu, Lampung-Indonesia. If s well known that the presence of corrosive gas either chlorine or sulfur in the steam atmosphere, noticeably increases the rates of corrosive greatly to high-temperatures corrosion [1–3]. One method of increasing the steel's resistance to chlorine attack is the here dip aluminizing. This method is both cheaper and more simple than other coating methods [4]. The aluminide layer formed on the steel can form the protective alumina layer (Al₂O₃) that it later protects the steel from severe oxidation attack during application for the electrical power plant [5]. Therefore, both production and maintenance cost for the steam pipelines system can be reduced and thus the electrical energy production is cheaper to being soon generated for people, industry, πc .

This study focused on the oxidation of aluminized AISI 1020 st 10 with NaCl deposit at 700 °C for 49 h in static air. This temperature is a high temperature limit that may be experienced by the components of steel ope. The reaction rate, morphology and corrosion product composition changes that occur on the aluminized steel were analyzed to provide insight into the mechanism of corrosion

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Experimental Procedure

5 The substates were cut into $\overline{20} \text{ mm} \times 10 \text{ mm} \times 2 \text{ mm}$ pieces from commercial AISI 1020 ste 6. The details of the specimen preparation and aluminizing process in the molten Al with a little Si bath at 700 °C for 16 s were similar to a previous study [5].

NaCl deposit was obtained by spraying 20 wt.% NaCl solution on the both of largest surface spectra placed on hot plate at 200 °C for 10 s. After NaCl deposition, the specimen was weighed and put into a mini crucible with size 4 5 mL and then exposed in the box furnace at 700 °C for a various time 1–49 h. Plot of the curve of weight gain versus oxidation time (h) is obtained to predict the oxidation resistance of bare steel and aluminized steel at 700 cz. Only the morphology, microstructure and chemical composition of the aluminized specimens are observed using Scanning Electron Microscopy (SEM) and Electron Dispersive Spectroscopy (EDS). Phases formed were examined by X-ray Diffraction (XRD).

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Results and Discussion

Oxidation Kinetics. Fig. 1a shows the 7 gh-temperature corrosion kinetics of both bare and aluminized steel at 700 °C. The bare steel not only had the highest weight gain, but also had been attacked severely by chlorine corrosion after 49 h. The weight gain of bare steel and aluminized steel with NaCl deposit is increased by factor of 1.5 and 16, respectively. For 49 h test, the weight gain of the aluminized steel exhibits the best corrosion resistance.

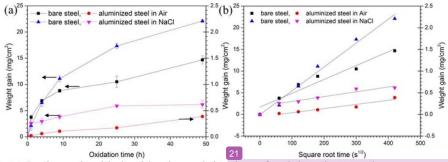


Figure 1. (a) Isothermal oxidation kinetics and (b) plots of weight gain per unit area vs. square root time for bare and aluminized AISI 1020 steel at 700 °C

The kinetics data $(W/A_o) = k_p t^n$, is plotted in Fig. 1b. According to near regression calculation from Fig. 1b, the kinetics rate (22) for the bare steel is $1.0256 \times 10^{-9} g^2 cm^{-4} s^{-1}$ and for the aluminized steel is $9.274 \times 10^{-13} g^2 cm^{-4} s^{-1}$ in air oxidioon. Whereas, the kinetics rate of bare and aluminized steel with NaCl deposit (3.034 $\times 10^{-9} g^2 cm^{-4} s^{-1}$ and $1.236 \times 10^{-10} g^2 cm^{-4} s^{-1}$, respectively. There was a substantial weight gain difference for the bare and the aluminized steel with/without NaCl deposit oxidized in static air for 49 h. The aluminide layer formed on the steel substrate gives best performace during high-temperature oxidation by forming the protective Al₂O₃ layer. However, the presence of chlorine leads to a fast corrosion rate and the degradation of alumina (Al₂O₃) layer fa²s to protect the steel substrate againts oxidant gas which contains chlorine because of continuously outward diffusion of Al to form Al₂O₃ and aluminum chlorides. Therefore, Spply Al-atoms from the aluminide layer is decreased to a lower Soncentration and Fe-atoms charges can diffuse out of iron rich areas to the further reaction in the formation of iron oxide nodules.

Microstructures and Corrogon Mechanisms. Aluminum top-coat and intermetallic layer consisting of Fe_2AI_5 and $FeAI_3$ on the steel substrate are the typical phases constitution after hot-dip in either pure-Al or Al with a little Si trait [4,5]. The experimental temperature (700 °C) in this stude was similar to a previous research and the phase constitution of the aluminized layers in our the aluminized AISI 1020 steel oxidized in static air for 1-9 h exposure, has been reported [5]. After oxidation in air for short-time exposure, Fe_2AI_5 and $FeAI_2$ were mainly framed in the aluminide layer at 700 °C, while FeAI were formed on the steel substrate [4–6]. Although the testing temperature in this study is lower than the melting point of NaCl (801 °C) [7]. According to Fig. 1b, the corrosion rate of aluminized steel is at least thr 3 orders of magnitude higher than that of air oxidation. Fig. 2a and 2b, respectively show the typical cross-sectional micrographs of aluminized steel after hot corrosion for 25 h and 49 h, indicating that NaCl induces hot corrosion of alloy and results in the formation of uniform attack in the aluminide layer.

SEM observation and EDS elements analysis of the aluminized specimen oxidized for 25 h (Fig. 2a) shows that the concentration of Cl (0.06 wt%) at the point 4 is lower than those of the point 2 (0.21 wt%) and 3 (0.13 wt%). The highest concentration of Cl (0.56 wt%) is detected at the point 1. The EDS e23 tents mapping examination of aluminized specimen corroded for 49 h (Fig. 2b) reveals that the outermost region of the external scale is rich in both iron and aluminum oxides (Fig. 2c), while some chlorides can be observed in the aluminide layer (Fig. 2d). Iron is relatively much

more detected in outermost region (Fig. 2e), while aluminum is nearly depleted in the external scale due to the formation of the volatile aluminum chlorides (AlCl₃) and inward diffusion into the steel substrate.

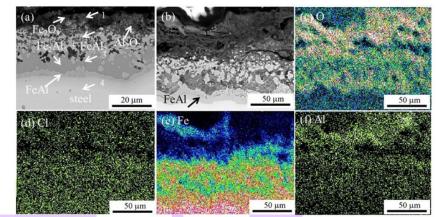


Figure 2. Cross-sectional SEM images of aluminized steel after oxidation (a) for 25 h, (b) 49 h at 700 °C, and (c-f) EDS map of elements O, Cl, Fe and Al on the cross sectional Fig. 2b

A different surface morphologies of aluminized steel after air oxidation and hot corrosion is shown in Fig. 3. For 4 h-air oxidation, the Fe_2Al_5 phase with a thin Al_2O_3 at the outerlayer can be observed using SEM and EDS examination (Fig. 3a). For a longer-oxidation (49 h), at the outer layer of the aluminide layer, only Al_2O_3 scale is detected by XRD and SEDM/EDS examinations, no iron oxide is found at outer layer (Fig 3b). It shows that the alumina scale gives the best protection of the AISI 1020 steel in air oxidation for 49 h.

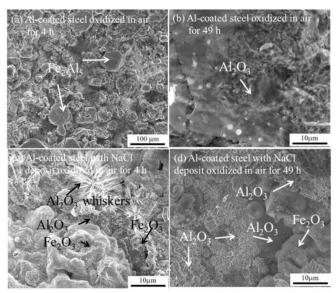


Figure 3. SEM Surface morphologies of aluminized AISI 1020 steel with/without NaCl deposit after oxidation test

Many studies [1–3] have reported the hot corrosion induced by NaCl deposits on Fe-Al base alloys that chlorine is the primary corrosive which accelerates species, the corrosion rate by forming volatile metallic chlorides. The increas 25 weight gain and the deposits of corrosion product on the surface of specimen during corrosion indicate that large amounts of Al-rich oxides and Fe-rich oxides are formed during corrosion. These oxides could be formed by a direct reaction bis veen

metal and oxygen and however should be considered. Fig. 3c shows the top view of scales formed after the 4-hr oxidation at 700 °C, implying that the scale is not protective and thus the corrosion rate in this stage becomes faster. XRD and EDS analysis reveal that the corrosion scale consists of mainly Al₂O₃, and Fe₂O₃ and a small and fint of FeCl₂. Aluminium chloride (AlCl₃) is not detected. In this study, Al₂O₃ whiskers and Fe₂O₃ grew on areas containing higher amounts of chlorine, such as cracks and voids of the surfaces of Al₂O₃ and Fe₂O₃ scales (Fig. 3c).

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The Al-oxide whiskers' growth implied that chlorine from $NaCl_{(s)}$ was present in the oxidizing atmosphere performing a catalyst role to increase the oxidation rate of the oxides in one direction. The growth of the Al_2O_3 whiskers is attributed to the vaporization of low melting point of $AlCl_3$ (182 °C) and high vapor pressure of the AlCl₃ [7], produced during the chloridation process of the aluminide layer: $2AI + 3Cl_{2(g)} = 2AICl_{3(g)}$ ($\Delta G_{700} = -471.6$ kJ). In addition, the Fe₂O₃ scale grows because a vacancies defects of Al₂O₃ can provide a rapid diffusion tunnel of oxygen for formation of Fe_2O_3 scale [4,8]. Since the high vapor pressure of AlCl₃ forced AlCl₃ to volatilize outward through voids or cracks in the $Fe_2Al_5 + FeAl_2$ layer 24 a high partial pressure of oxygen environment, causing verifiester growth Al_2O_3 by reaction: $4AlCl_{3(g)} + 3O_{2(g)} = 2Al_2O_{3(s)} + 6Cl_{2(g)}$ $(\Delta G_{700} = -592.4 \text{ kJ})$. Meanwhile, oxygen in the atmosphere can penetrate through the interconnected voids and cracks into the aluminide layer and leads to the Al₂O₃ whisker being gradually replaced by the uniform growing Al₂O₃ scale (Fig. 3d) due to the fact that the driving force for oxidation is higher than that for chloridation [8]. Similarly, the chloridation/oxidation reaction of Fe₂O₃ formation, is $2Fe + 3Cl_{2(g)} = 2FeCl_{3(g)} (\Delta G_{700} = -157.5 \text{ kJ})$, and the followed by evaporation of volatile FeCl₃. The FeCl_{3(g)} is converted into iron oxide by reaction: $4FeCl_{3(g)} + 3O_{2(g)} = 2Fe_2O_3 + 3O_{2(g)} = 2Fe_2O_2 + 3O_{2(g)} = 2Fe_2O_2 + 3O_{2(g)} = 2Fe_2O_$ $6Cl_{2(g)}$ ($\Delta G_{700} = -109.3$ kJ). In addition, some chlorine is generated by both the oxidation of AlCl₃ and FeCl₃ can penetrate back into the aluminide layer to trigger oxidation/chloridation cyclic reactions and later destroys the aluminide layer after long-term oxidation (see in Fig. 2b). Fe-rich oxide nodules grow with the Al₂O₃ scale and thus the protective Al₂O₃ layer fails to protect the steel. Therefore, the weight gain of specimen is increased (Fig .1a).

Summary

The presence of NaCl in deposits inhibits the formation of protective oxide scale, leading to the acceleration of hot corrosion of aluminized Aler. 1020 steel. Corrosion products are found to be Al₂O₃, Fe₂O₃ nodules, and FeCl₂. The depletion of aluminum in the aluminide layer is caused by the evaporation of AlCl₃, and continuously increases the corrosion rate and the degradation of the aluminide layer. A rapid Fe-oxide nodules' growth and a amount of aluminum oxide formation significantly result an increase in weight gain of the aluminized specimen.

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